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C L A I M S

1. Process to prepare a haze free base oil having a cloud point of below 0 °C and a kinematic viscosity at 100 °C of greater than 10 cSt by performing the following steps:

- 5       (a) hydroisomerisation of a Fischer-Tropsch synthesis product,
- (b) isolating one or more fuel products and a distillation residue,
- (c) reducing the wax content of the residue by contacting  
10      the feed with a hydroisomerisation catalyst under hydroisomerisation conditions, and
- (d) solvent dewaxing the product of step (c) to obtain the haze free base oil.

2. Process according to claim 1, wherein the  
15      distillation residue has a 10 wt% recovery boiling point of above 500 °C and a wax content of greater than 50 wt% and wherein in step (c) the wax content is reduced to a value below 50 wt%.

3. Process according to any one of claims 1-2, wherein  
20      the wax content in step (c) is reduced to below 35 wt%.

4. Process according to claim 3, wherein the wax content in the product of step (c) is between 10 and 35 wt%.

5. Process according to any one of claims 1-4, wherein  
25      the Fischer-Tropsch synthesis product has a weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product is at least 0.2 and wherein at least 30 wt% of compounds in the Fischer-Tropsch synthesis product have at least 30 carbon atoms.

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6. Process according to claim 5, wherein at least 50 wt% of compounds in the Fischer-Tropsch product have at least 30 carbon atoms.

5 7. Process according to any one of claims 5-6, wherein the weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product is at least 0.4.

8. Process according to any one of claims 1-7, wherein the 10 wt% recovery boiling point of the residue as 10 isolated in step (b) is between 350 and 550 °C.

9. Process according to any one of steps 1-8, wherein more than 50 wt% of the product of step (c) boils above the 10 wt% recovery point of the residue used as feed in step (c).

15 10. Process according to claim 9, wherein more than 70 wt% of the product of step (c) boils above the 10 wt% recovery point of the residue used as feed in step (c).

11. Process according to any one of claims 1-10, wherein the hydroisomerisation catalyst used in step (c) is a 20 substantially amorphous based catalyst comprising a silica-alumina carrier and a noble or non-noble Group VIII metal.

12. Process according to any one of claims 1-10, wherein the hydroisomerisation catalyst used in step (c) 25 comprises a molecular sieve and a noble or non-noble Group VIII metal.

13. Process to prepare a lubricant composition not containing a viscosity modifier additive by blending a low viscosity base oil with the haze free base oil as 30 obtained in step (d) of the process as described in claims 1-12 and one or more additives.